Effects of -NO2 and -NH2 functional groups in mixed-linker zr-based MOFs on gas adsorption of CO2 and CH4

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Original Research

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ABSTRACT

This study was undertaken to evaluate the effects of mixing BDC-NO2 and BDC-NH2 linkers in the synthesis of Zr-based metal organic frameworks (Zr-MOFs) on their adsorption and separation of CO2 and CH4. UiO-66 with single or binary -NO2 and -NH2 samples were synthesized under solvothermal conditions and activated by solvent exchanging using methanol. Structural analyses of the materials were conducted using FTIR, XRD, TGA, SEM, 1HNMR and N2 adsorption/desorption techniques and adsorption of CO2 and CH4 at high pressures and different temperatures (273 and 298 K) was investigated. It was found that UiO-66-NH2 exhibited higher CO2 and CH4 adsorption capacities than those of UiO-66-NO2. Addition of -NH2 functional group in UiO-66-NO2 could enhance CO2 and CH4 adsorption due to the extra CO2 adsorption sites of -NH2 functional groups. Addition of -NO2 functional group to UiO-66-NH2 at a low loading could also increase CO2 and CH4 adsorption, however, a high loading of NO2 functional group to UiO-66-NH2 would result in decreased adsorption.

1. Introduction

Capture and separation of carbon dioxide from methane is one of major process for high-valued methane utilization. The effective separation of carbon dioxide (CO2) from methane (CH4) can be achieved through some technologies. Adsorption based separation technology such as physical adsorption by porous materials is considered to be a cost efficient process and many types of adsorbent materials have been examined, such as activated carbon, zeolites and metal organic frameworks (MOFs) [1–8].

Metal organic frameworks (MOFs) are a new class of crystalline and promising porous materials, which have recently attracted considerable interest in many applications for gas adsorption and storage, due to their high specific surface area and pore volume. Until now, numerous MOFs have been synthesized and studied in capture of CO2, storage of CH4 and their separation [9,10]. Mg-MOF-74, zeolitic imidazolate frameworks (ZIFs) and bio-MOF-11 have showed high CO2 adsorption [11–13]. For methane storage, Ni-MOF-74 [14–16], MOF-177 [17] and PCN-14 [18] have been demonstrated good capacities.

The uptake capacities of CO2 and CH4 on MOFs are dependent on the structural properties such as pore volume and surface area of MOFs. However, achieving a highly selective uptake of a specific gas on MOFs, a balanced porosity and functionality of the framework should be considered [10]. In addition, different types of functional groups (Br, CH3, NO2, NH2, etc.) in the structure of MOFs [19,20] also affect the surface area and adsorption. Ying et al. stated that NH3 group can show a good role and provide strong affinity for CO2 molecules in the adsorption [21]. And NO2 group can also play as Lewis basic sites to increase CO2 adsorption by acid-base interactions [22].

Many functionalized MOFs [23] have been shown as good adsorbents for CO2 and CH4 uptakes [24–26]. Amino (NH2)-functionalized MOFs usually displayed an improvement in separation of CO2/CH4 [27,28] whereas nitro (NO2) functionalized MOFs reduced surface area and CO2/CH4 adsorption [29].

Recently, combination of two different ligands (functional group or non-functional group) over MOFs have been studied by some researchers [30]. The MOFs were referred as mixed linker MOFs (MixMOFs). The properties of MixMOFs led them to be promising sorbent
materials for CO2 and CH4 adsorption, such as Al-MIL-53, CAU-10 [31], Ti-based MOFs [32] and UiO-66 [33] mixed linker MOFs. More recently, UiO-66 mixed linker MOFs have been studied by two research groups due to their high thermal and chemical stabilities. Kim et al. [34] synthesized a mixture of BDC-NH2 and Br-BDC functionalized UiO-66-Br-NH2. A mixture of BDC (non-functional linker) with BDC-NH2 at different loadings functionalized UiO-66 has been studied by Chavan et al. [33].

In this article, for the first time, BDC-NO2 and BDC-NH2 functionalized linkers at different loadings were used for preparation of MixMOFs of UiO-66 and their physicochemical properties and performances in CO2 and CH4 adsorption were characterized and compared with single functionalized UiO-66-NO2 and UiO-66-NH2.

2. Experimental section

2.1. Chemicals and synthesis of different UiO-66 samples

All chemicals including zirconium chloride (ZrCl4, 99.9%), N, N-dimethylformamide (DMF, CH3NO, 98%), methanol (CH3OH, 99%), 2-nitroterephthalic acid (BDC-NO2, ≥ 99%), and 2-aminoterephthalic acids (BDC-NH2, 99%) were supplied by Sigma-Aldrich without further purification.

UiO-66-NO2 was synthesized based on the previous reports [35]. In a typical process, ZrCl4 (6.5 mmol) was dissolved in DMF (86 mL) in a Teflon vessel and stirred for 10 min. BDC-NO2 (6 mmole) was then added to the solution and stirred for 20 min. The homogeneous mixture was placed in a Parr PTFE-lined digestion vessel of 125 mL, sealed and left in an oven for 24 h at 393 K. The product was washed two times with DMF and filtered by vacuum filtration. UiO-66-NH2 was obtained by the similar synthesis procedure of UiO-66-NO2 using a BDC-NH2 linker instead of BDC-NO2.

Synthesis of mixed linker UiO-66-NO2-N (N = NH2) and UiO-66-NO2-N (N = NO2) were achieved by using the above process through different ratios of the two linkers, BDC-NO2 and BDC-NH2 as described in Table S1 (ESI). The molar fractions of BDC-NH2 with respect to BDC-NO2 were at 0.10 and 0.75 for UiO-66-NO2-N samples and vice versa for UiO-66-NH2-N samples, and the linker BDC-NO2 with respect to BDC-NH2 were also at 0.10 and 0.75.

Activation of all samples were carried out using the method as previously reported [35]. About 0.5 g of each sample was immersed separately in 50 mL of methanol solution for 5 d and then the solids were filtered and dried in an oven at 353 K for 12 h. Finally, these materials were heated under vacuum at 463 K overnight.

2.2. Characterisation of samples

The crystalline structure of samples was confirmed by a XRD diffractometer (D8 Advance-diffractometer Bruker X8) with Cu Ka radiation (λ = 1.5406 Å). A FTIR spectrometer (Perkin-Elmer 100 FT-IR spectrometer) was used to investigate functional groups on MOF crystalline structure. The spectrum was scanned from 600 to 4000 cm⁻¹ with a resolution of 4 cm⁻¹ by using an attenuated total reflectance (ATR) technique. Thermal stabilities of all samples were investigated by using a thermogravimetric analysis (TGA) instrument (TGA/DSC1 STAR® system, METTLER-TOLEDO). About 10–20 mg samples were loaded in an alumina pan and then argon gas was introduced into the furnace at a flow rate of 20 mL/min and a heating rate of 10 K/min from 308 to 1150 K. A SEM machine (Zeiss NEON 40 EsB Cross-Beam) was used to determine the morphologies of the samples. Surface area and pore size of each sample were measured by a Micromeritics Tristar 3000 analyzer. All samples were degassed at 463 K under vacuum overnight and then N2 adsorption at 77 K was carried out. 1H NMR spectroscopy was used to detect the incorporation of the linkers BDC-NO2 and BDC-NH2 into MOF samples. About 20 mg of samples were digested in 600 μL of NaOH-D2O solution for 24 h before the measurement. The data were recorded on a Bruker Advance III 400 spectrometer and were indirectly referenced to TMS using the resonance of the residual solvent peak.

2.3. Adsorption study of CO2 and CH4

A Micromeritics ASAP2050 was used to measure the adsorption isotherms of pure CO2 (99.995%) and CH4 (99.995%) at high pressure up to 1000 kPa on samples. Carbon dioxide (99.995%) and methane (99.995%) were supplied by Coregas. First, the samples were thoroughly dehydrated and degassed on the Micromeritics ASAP2050 analyzer by heating stepwise at 1 K/min up to 423 K and holding at this temperature for 8 h under high vacuum. An equilibrium interval of 20 s was adopted in all the isotherm measurements. The adsorption was carried out at temperatures of both 273 and 298 K.

3. Results and discussion

Fig. 1 shows XRD patterns of as-synthesized UiO-66-NO2-N, UiO-66-NH2-N, UiO-66-NO2 and UiO-66-NH2 samples.

Fig. 2 and 3 show FTIR spectra of non-activated and activated
samples. The functional carboxyl in free aromatic carboxylic acid on non-activated samples was observed at 1650 cm\(^{-1}\). However, after activation of the samples by methanol, the peak was mostly disappeared, demonstrating that a good exchange of DMF by methanol. [39] The asymmetric (\(\nu(\text{NO})_{\text{asym}}\)) peak at 1544 cm\(^{-1}\) reduced and disappeared at loading of 10% and 75% (-NH\(_2\)) group to UiO-66-NO\(_2\), meanwhile the C-N stretching of aromatic amines appeared at 1356 cm\(^{-1}\) on both the samples of UiO-66-NO\(_2\)-NH\(_2\)-10% and UiO-66-NO\(_2\)-NH\(_2\)-75% [33]. In contrast, the asymmetric (\(\nu(\text{NO})_{\text{asym}}\)) vibration at 1544 cm\(^{-1}\) appeared on mixed linker samples and the C-N stretching of aromatic amines at 1356 cm\(^{-1}\) was missing at the loading 10% and 75% of (-NO\(_2\)) group to UiO-66-NH\(_2\) samples. A similar behavior was observed for the symmetric (\(\nu(\text{NO})_{\text{sym}}\)) stretching at 1355 cm\(^{-1}\), which decreased after loading the UiO-66-NO\(_2\) sample with (-NH\(_2\)) group and vice versa with the addition of (-NO\(_2\)) groups to the sample UiO-66-NH\(_2\) [40,41].

The \(^1\)H NMR spectra of synthesized samples are shown in Fig. 4. As it can be seen that, BDC-NH\(_2\) and BDC-NO\(_2\) linkers can be found in UiO-66-NH\(_2\) and UiO-66-NO\(_2\), respectively [38]. For the mixed-linker UiO-66-NO\(_2\)-NH\(_2\), both BDC-NH\(_2\) and BDC-NO\(_2\) linkers were found. As expected, by increasing the amount of BDC-NH\(_2\) linker into UiO-66-NO\(_2\) sample, the signals of BDC-NH\(_2\) become more visible in samples of UiO-66-NO\(_2\)-NH\(_2\)-10% and UiO-66-NO\(_2\)-NH\(_2\)-75% and vice versa with increased BDC-NO\(_2\) linkers to UiO-66-NH\(_2\) samples. The intensities of BDC-NO\(_2\) signals in UiO-66-NH\(_2\)-NO\(_2\)-10% and UiO-66-NH\(_2\)-NO\(_2\)-75% samples were obviously presented. Thus, \(^1\)H NMR spectra clearly proved the incorporation of the linkers into the frameworks of the samples.

The thermal stability of samples was examined by TGA and weight loss profiles are presented in Fig. 5. DTG profiles of all samples are illustrated in Fig. S3. The TGA curves of non-activated samples showed three-steps of weight losses. The first step of the weight loss at 5 \(\sim\) 8% occurred from 305 to 375 K and it is attributed to the removal of moisture and free solvent inside the pores [42]. Meanwhile, the second weight loss at 23 \(\sim\) 30% took place in the range of 375 \(\sim\) 460 K and this loss is related to the removal of un-coordinated linkers and coordinated solvent (DMF), due to the strong chemical bonding. The last stage (third-step) of weight loss at 62 \(\sim\) 72% is referred to the structural collapse of the MOF samples occurring at 760 K. Fig. 5(b) shows the TGA results for activated samples. It can be confirmed that weight losses appear on all samples with slight differences in the non-activated samples. The removal of moisture and free solvent (initial step) happened at 350 K with 12 \(\sim\) 22% weight loss. However, the second step of weight loss on activated samples presented very small amount of 5% loss compared with the non-activated samples. This provides the evidence of successful exchange of the solvent [33]. The decomposition temperature of activated samples slightly increased to 820 K, suggesting their higher thermal stability.

Fig. 6 presents N\(_2\) adsorption/desorption isotherms at 77 K. A different hysteresis was observed in all samples, which indicates the presence of mesoporous structure with the micropores. A similar observation on functionalized UiO-66 samples has been reported previously [33]. The BET surface areas, micropore volumes and areas of the samples by the t-plot method are presented in Table S2 (ESI). The surface areas can be increased at the lower loading of a second linker but declined with further increasing loading of the functional linkers to UiO-66-NH\(_2\) or UiO-66-NO\(_2\) samples. UiO-66-NO\(_2\)-NH\(_2\)-10% and UiO-66-NH\(_2\)-NO\(_2\)-10% displayed higher surface areas at 867 m\(^2\)g\(^{-1}\) and 1000 m\(^2\)g\(^{-1}\) respectively.
1152 m\(^2\)g\(^{-1}\) than single linker functionalized samples, UiO-66-NO\(_2\) and UiO-66-NH\(_2\) at 771 m\(^2\)g\(^{-1}\) and 1025 m\(^2\)g\(^{-1}\), respectively. More specifically, BDC-NO\(_2\) linker has the least favorable energy of structural assembly because of the electronegative -NO\(_2\) group. Adding few amount of BDC-NH\(_2\) linker may enhance the formation of the structure of UiO-66-NH\(_2\) itself and the solvent\([43]\). Therefore, adding few amount of BDC-NH\(_2\) as a second linker at different polarities of the ligands\([48]\).

Suitable sizes of micropores within MOF structure also affect the selectivity towards \(\text{CO}_2\) with less interconnection\([56]\). The quadrupole moment of \(\text{CO}_2\) \((-13.4\times10^{-40} \text{ C.m}^2\)\) creates strong interactions with adsorbents. Suitable sizes of micropores within MOF structure also affect \(\text{CH}_4\) molecular adsorption\([57]\).

The selectivity of \(\text{CO}_2\) over \(\text{CH}_4\) by the static adsorption at pressure up to 1000 kPa was calculated according to Eq. S1 and displayed in Fig. 10. UiO-66-NH\(_2\) gave a better selectivity than UiO-66-NO\(_2\). Addition of a second linker BDC-NO\(_2\) to UiO-66-NH\(_2\) improves the selectivity while addition of BDC-NH\(_2\) to UiO-66-NO\(_2\) can result in a lower selectivity because the electron withdrawing nature of the nitro group would be expected to strongly impact coordination where the nitro...
group affected the sorption of protic guests [58]. Consequently, the N-based Lewis basic functional polar surfaces in the framework may also lead to the high CO2 selectivity [56]. At pressure of 1000 kPa, UiO-66-NO2-NH2 75% has the lowest separation factor for carbon dioxide over methane (2.05) and (2.16) at 298 K and 273 K, respectively, whereas, UiO-66-NH2-NO2 10% displays the best selectivity amongst others. The selectivity of CO2 over CH4 decreased with increasing pressure.

Therefore, the selectivity of CO2 /CH4 of most samples at pressure lower than 200 kPs can be selected as best separation. Table 2 summarizes the selectivity of CO2 over CH4 on various MOFs. The selectivities of CO2 over CH4 for mixed ligands MOFs are better in comparison with other MOFs.

In Figs. S4 and S5 (ESI), the isosteric heats of adsorption (\(Q_{st}\)) for CO2 and CH4 were determined based on the Clausius–Claperyon
equation \( dp/p = \Delta H dT/RT^2 \) from isotherms that measured at 273 and 298 K. Generally, CO\(_2\) isosteric heats of adsorption slightly reduced with increasing coverage of CO\(_2\) on samples. UiO-66-NO\(_2\) showed the lowest value due to a larger pore size [60]. The adsorption heat of CO\(_2\) adsorption at different CO\(_2\) loading on samples were found at an average between 28 and 33 kJ/mol, which are in the range of heat of adsorption of most MOFs. On the other hand, the average adsorption heat values of CH\(_4\) at different CH\(_4\) coverages were between 18 and 29 kJ/mol on samples. Similar to the previous work, the isosteric heat of CH\(_4\) increased on samples with high loading of CH\(_4\), relating to more dispersion of CH\(_4\) occurring on the polar surface [61].

4. Conclusions

Multifunctionalized Zr-based MOFs samples (UiO-66-NO\(_2\), UiO-66-NO\(_2\)-NH\(_2\) 10%, UiO-66-NO\(_2\)-NH\(_2\)-NO\(_2\) 75%, UiO-66-NH\(_2\), UiO-66-NH\(_2\)-NO\(_2\) 10% and UiO-66-NH\(_2\)-NO\(_2\) 75%) were obtained for CO\(_2\) and CH\(_4\) adsorption. 1H NMR and FTIR indicate the good incorporation of the two functional groups of BDC–NO\(_2\) and BDC–NH\(_2\) in MOF structures. Uptake capacities of CO\(_2\) and CH\(_4\) on UiO-66-NH\(_2\)-NO\(_2\) 10% were the highest around 6.6 and 9.1 mmol CO\(_2\)/g at 298 and 273 K, respectively, and 2.5 and 3.5 mmol CH\(_4\)/g, at 298 and 273 K, respectively. UiO-66-NO\(_2\)-NH\(_2\) 75% presented the lowest of CO\(_2\) and CH\(_4\) adsorption. Overall, mixed ligands MOFs demonstrated good adsorption of CO\(_2\) and CH\(_4\), however, selectivity of CO\(_2\)/CH\(_4\) could be reduced.

Acknowledgements

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Appendix A. Supporting information

Supplementary data associated with this article can be found in the
Table 2
Separation selectivity of CO2/CH4 on various MOFs.

<table>
<thead>
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<th>MOFs</th>
<th>CO2/CH4 at 298 K</th>
<th>CO2/CH4 at 273 K</th>
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<td>3.8 (1 bar) 2.7</td>
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<td>(9.8 bar)</td>
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<tr>
<td>UiO–66–NH2</td>
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<td>3.5 (1 bar) 2.3</td>
<td>This work</td>
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<td>(9.8 bar)</td>
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<tr>
<td>ZIF 68</td>
<td>3.8 (1 bar) 5.0</td>
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<td>[59]</td>
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<tr>
<td>UiO–66–NH2NO2 75%</td>
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<td>3.4 (1 bar) 2.4</td>
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<td>3.1 (1 bar) 2.2</td>
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<td>UiO–66–NH2NO2 10%</td>
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<td>3.4 (1 bar) 2.2</td>
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This work

References


